

RG

Stratified Turbulence

7/31/2019

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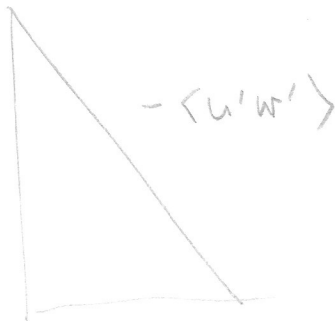
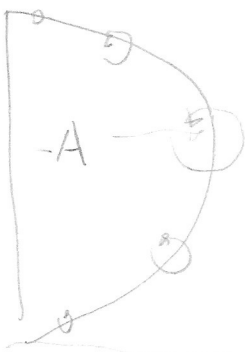
Review of unstratified b.l. turbulence

Key empirical findings:

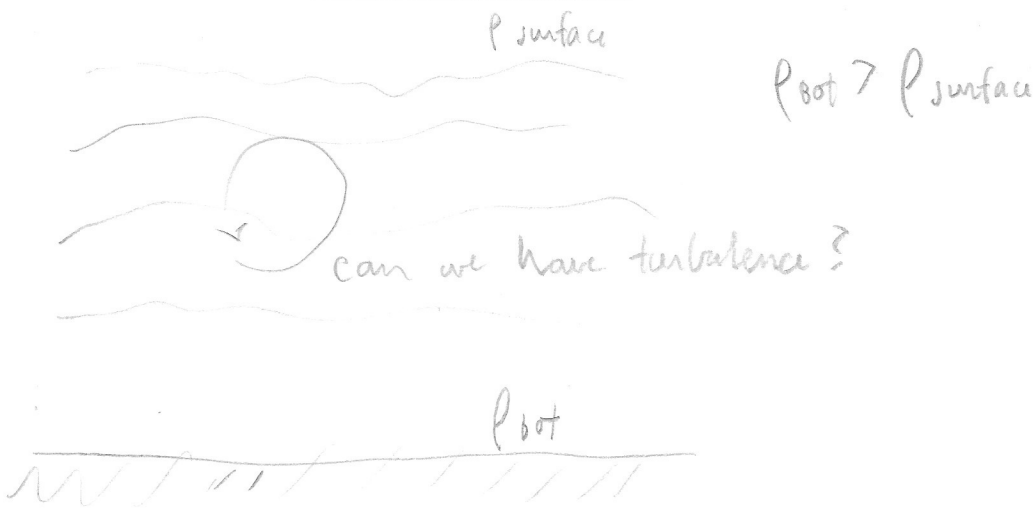
- 1) Quadratic drag
- 2) Log Layer
- 3) Eddy Viscosity

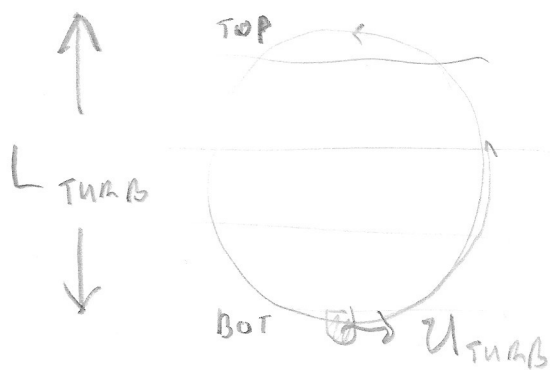
$$A = u_{TURB} L_{TURB}$$

$$u_{TURB} = |\langle u'w' \rangle|^{1/2}, \quad L_{TURB} \approx K z \left(1 - \frac{z}{h}\right)^{1/2}$$



Now with stratification





if the parcel doesn't have enough energy to turn over then it is an internal wave

KE = $\frac{1}{2} U_{TURB}^2$, Bernoulli = $\frac{1}{2} u^2 + p' = B$

change of PE = $\frac{1}{2} \Delta \rho g L_{TURB}$ $\Delta \rho = \rho_{BOT} - \rho_{TOP}$

$\frac{1}{2} \bar{\rho} U_{TURB}^2 = \frac{1}{2} \Delta \rho g L_{TURB}$

substitute in: $N^2 = -\frac{g}{\bar{\rho}} \frac{\partial \rho}{\partial z}$ fastest frequency² of internal waves

$\Rightarrow U_{TURB}^2 = N^2 L_{TURB}^2$

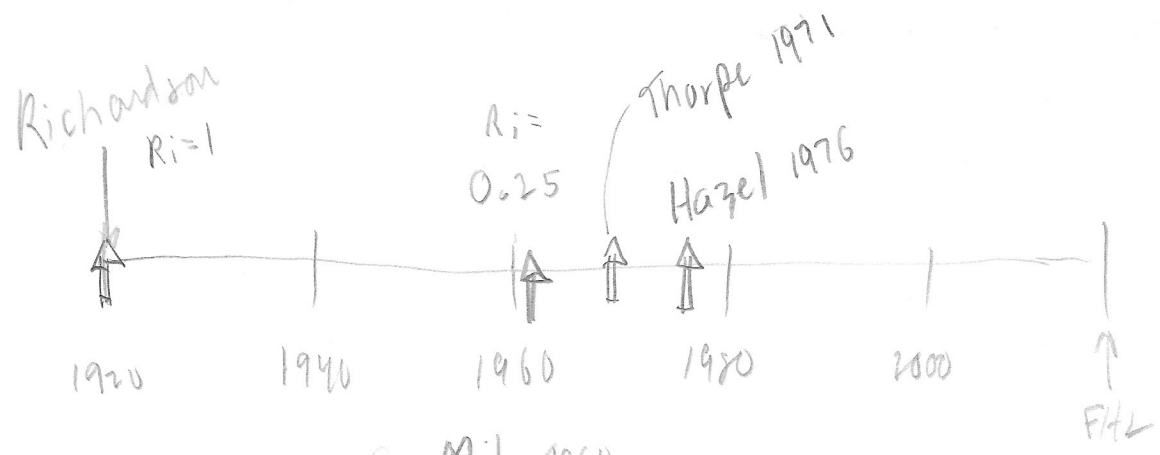
OR $L_{TURB} \leq U_{TURB} / N$

if we satisfy the inequality then the wheel can turn over and the flow is turbulent

$\approx \frac{N^2}{U_{TURB}^2 / L_{TURB}^2} < 1$

shear of turbulence: assume it is proportional to the square of the mean shear

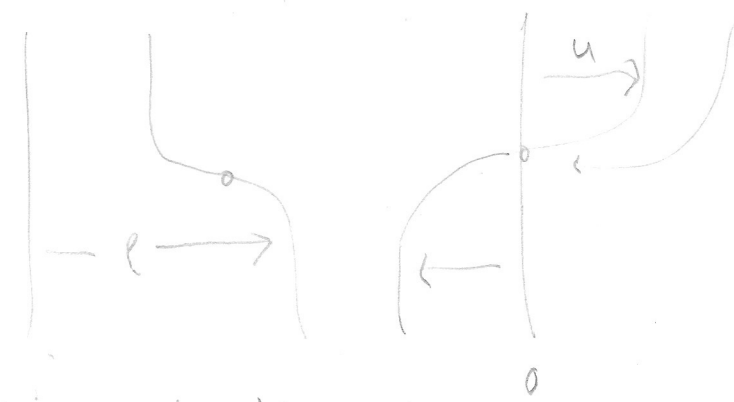
$\Rightarrow \frac{N^2}{(\frac{\partial \langle u \rangle}{\partial z})^2} < 1 \equiv \text{Richardson \#} , Ri$
really gradient Richardson #



$R_i > 0.25$ flow is stable

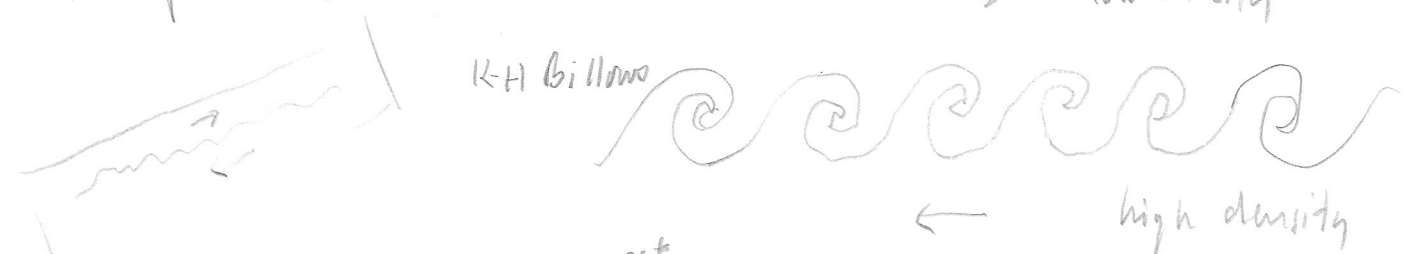
$R_i < 0.25$ Necessary but not sufficient condition for flow to be unstable

Hazel



if min R_i is at the inflection point then $R_i = 1/4$ is sufficient.

Thorpe Experiments = tilt tank



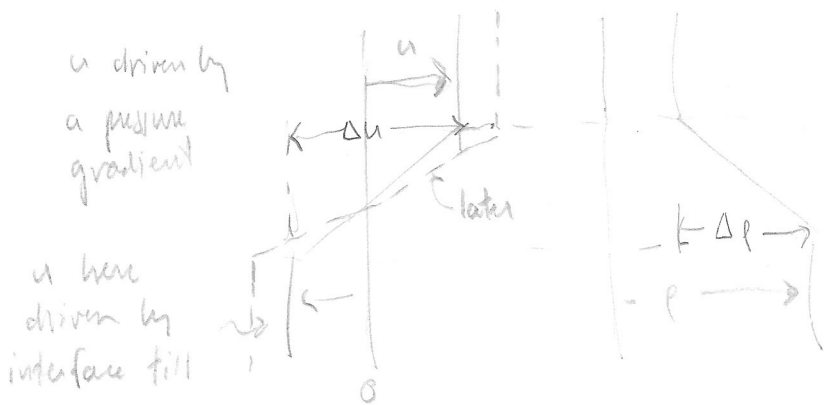
growth rate $\alpha = \alpha_0 e^{\alpha t}$

$$\alpha = \frac{\partial u_z}{\partial z} 0.2 (1 - 4R_i)$$

$\Rightarrow 0$ at $R_i = 1/4$

Marginally Critical Stratified Turbulence

Thought experiment: forced shear layer: u is accelerating



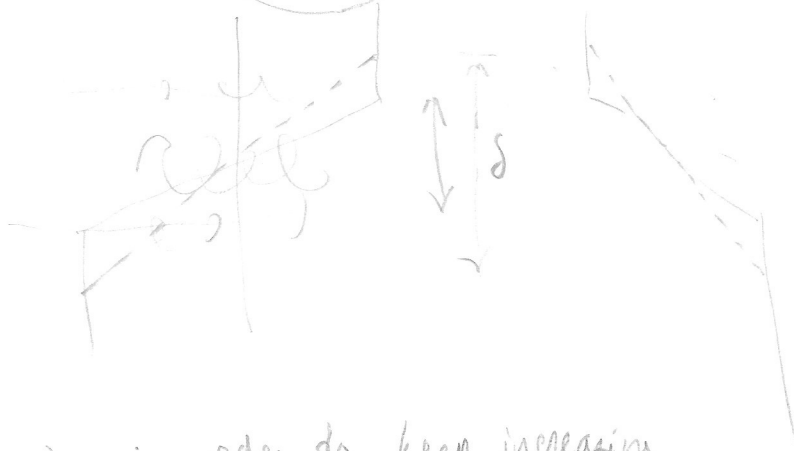
u driven by a pressure gradient

u here driven by interface tilt

Imagine $Ri > \frac{1}{4}$

Then shear will increase while stratification is unchanged

when Ri goes to $\frac{1}{4}$ there will be turbulent mixing layer entrains + gets thicker



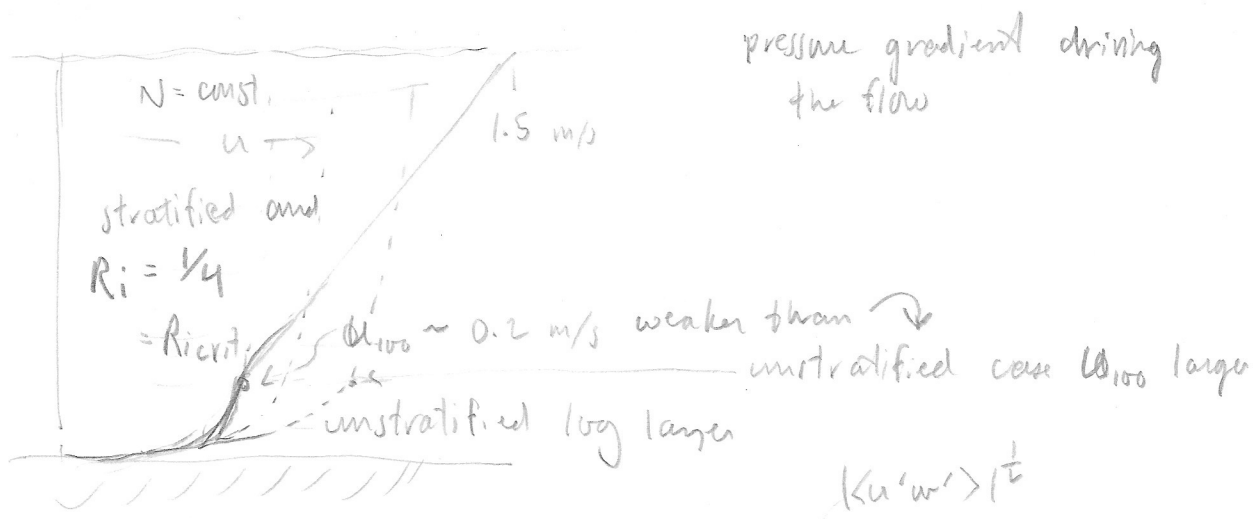
$$\frac{\Delta p g \delta}{(\Delta u)^2} = 0.25 \quad (*)$$

$$\approx \frac{\Delta p g}{\rho \cdot \delta} \cdot \delta$$

$$= \frac{\Delta p g}{(\Delta u / \delta)^2}$$

(*) \Rightarrow in order to keep increasing Δu while maintaining $Ri = \frac{1}{4}$ Requires that δ get thicker.

Entrainment means advection of fluid from a region without mixing into a region with mixing.



$$A = L_{TURB} U_{TURB} = \frac{-\langle u'w' \rangle}{\partial u / \partial z} = \frac{U_{TURB}^2}{Ri_{crit}^{1/2} N}$$

$$Ri_{crit} = \frac{N^2}{(\partial u / \partial z)^2} = 0.25$$

$$\Rightarrow L_{TURB} = Ri_{crit}^{1/2} \frac{U_{TURB}}{N} = 0.5 \frac{U_{TURB}}{N}$$

$$\approx L_{TURB} = 0.5 \frac{u_*}{N}$$

This is close to the Ozmidov scale

$$L_0 = \left(\frac{\epsilon}{N^3} \right)^{1/2}$$

Just need to estimate ϵ (dissipation) for the b.l. case above

Invoke = Production of TKE $\equiv \epsilon + \frac{g}{\rho} \langle \rho' w' \rangle$
 called "efficiency" ≈ 0.2
 Buoyancy Flux

$$\frac{Buoy}{\epsilon} = \text{efficiency} \approx 0.2$$

$$\frac{Buoy}{Prod} = R_f \text{ really is efficiency} \approx 0.167$$

6

$$\text{Prod} = - \langle w'w' \rangle \frac{\partial u}{\partial z}$$

$$\varepsilon = (1 - R_f) \langle w'w' \rangle \frac{\partial u}{\partial z}$$

$$\Rightarrow \frac{\varepsilon}{N^3} = (1 - R_f) Ri^{-\frac{1}{2}} \frac{U_{\text{TURB}}^2}{N^2}$$

$$L_0 = \left(\frac{\varepsilon}{N^3} \right)^{\frac{1}{2}} = (1 - R_f)^{\frac{1}{2}} Ri^{-\frac{1}{4}} \frac{U_{\text{TURB}}}{N}$$

↑ similar to the overturn scale (Thompson scale)

∩ turbulence